

3-5 有熱源的問題

有時候，材料內某些型式的能量會轉變為熱能，如電能、化學能及核能等，此時，可視為內部有熱源。當吾人處理一維、穩態且有熱源的問題時，其統御方程式（熱擴散方程式）為

$$\frac{1}{r^n} \frac{\partial}{\partial r} \left(kr^n \frac{\partial T}{\partial r} \right) + \dot{g} = 0 \quad (3-5.1)$$

其中 $n = \begin{cases} 0 : \text{直角座標} \\ 1 : \text{圓柱座標} \\ 2 : \text{球座標} \end{cases}$

\dot{g} 為單位體積的熱源。

若 k 為常數，則上式變成

$$\frac{1}{r^n} \frac{\partial}{\partial r} \left(r^n \frac{\partial T}{\partial r} \right) + \frac{\dot{g}}{k} = 0 \quad (3-5.2)$$

吾人以直角及圓柱座標分別討論如下：

1. 平面牆

(3-5.2) 變成

$$\frac{d}{dx} \left(\frac{dT}{dx} \right) + \frac{\dot{g}}{k} = 0$$

積分

$$\frac{dT}{dx} = \int \frac{-\dot{g}}{k} dx$$

再積分

$$T = \int \left(\int \frac{-\dot{g}}{k} dx \right) dx$$

若 \dot{g} 為常數，則溫度分布之通解為

$$T = -\frac{\dot{g}}{2k}x^2 + c_1x + c_2 \quad (3-5.3a)$$

將 B.C's 代入，即可求得 c_1 與 c_2 ，且 \dot{q}_x 可得

$$\dot{q}_x = -k \frac{dT}{dx} = \dot{g}x - c_1k \quad (3-5.3b)$$

2. 圓柱 (管長 L)

(3-5.2) 變成

$$\begin{aligned} \frac{1}{r} \frac{d}{dr} \left(r \frac{dT}{dr} \right) + \frac{\dot{g}}{k} &= 0 \\ \Rightarrow \frac{d}{dr} \left(r \frac{dT}{dr} \right) &= -\frac{\dot{g}r}{k} \end{aligned}$$

積分

$$\begin{aligned} r \frac{dT}{dr} &= \int -\frac{\dot{g}r}{k} dr \\ \Rightarrow \frac{dT}{dr} &= \frac{1}{r} \int -\frac{\dot{g}r}{k} dr \end{aligned}$$

再積分

$$T = \int \left(\frac{1}{r} \int -\frac{\dot{g}r}{k} dr \right) dr$$

若 \dot{g} 為常數，則溫度分布之通解為

$$T = -\frac{\dot{g}r^2}{4k} + c_1 \ln r + c_2 \quad (3-5.4)$$

將 B.C's 代入，即可求得 c_1 與 c_2 。對實心圓柱而言，當 r 趨近於 0 時， $\ln r$ 趨近於 $-\infty$ ，故 $c_1 = 0$ ，上式變成

$$T = -\frac{\dot{g}r^2}{4k} + c_2 \quad (3-5.5a)$$

而 \dot{q}_r 及 \dot{Q}_r 分別為

$$\dot{q}_r = -k \frac{dT}{dr} = \frac{\dot{g}r}{2} \quad (3-5.5b)$$

$$\dot{Q}_r = \dot{q}_r (2\pi r L) = \dot{g} \pi r^2 L = \dot{g} \nabla_r \quad (3-5.5c)$$

其中 ∇_r 為半徑 r 之圓柱體積。



例題 3

Consider the plane wall with uniformly distributed heat sources shown in figure. The thickness of the wall in the x direction is $2L = 2$ m, A current passing through this conducting material with the heat generated per unit volume is $\dot{q} = 200$ W/m³, and assume the thermal conductivity $k = 10$ W/m·K does not vary with temperature, the differential equation which governing the heat flow is

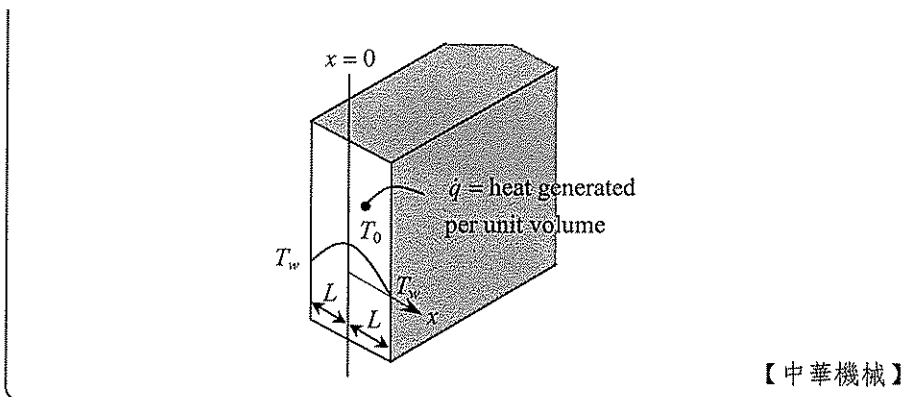
$$\frac{d^2T}{dx^2} + \frac{\dot{q}}{k} = 0$$

For boundary conditions either side of the wall temperature, $T_w = 30^\circ\text{C}$ at $x = +L, -L$.

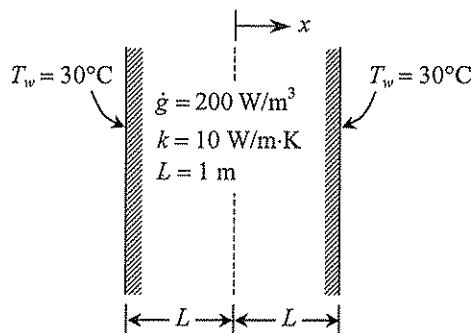
Determine:

(1) the temperature of the midplane, T_0

(2) the temperature distribution, $\frac{(T - T_w)}{(T_0 - T_w)}$ (15%)



解：



由題意可知，熱擴散方程式為

$$\frac{d^2T}{dx^2} + \frac{\dot{g}}{k} = 0$$

積分兩次可得通解為

$$T(x) = -\frac{\dot{g}}{2k}x^2 + c_1x + c_2$$

而 B.C's 為

$$\begin{cases} T(-L) = T_w \\ T(L) = T_w \end{cases}$$

故 c_1 及 c_2 分別為

$$c_1 = 0$$

$$c_2 = \frac{\dot{q}L^2}{2k} + T_w$$

因此，溫度分布為

$$T(x) = \frac{\dot{q}L^2}{2k} \left(1 - \frac{x^2}{L^2}\right) + T_w$$

$$\begin{aligned} (1) \quad T_0 = T(x=0) &= \frac{\dot{q}L^2}{2k} + T_w = \frac{200(1)^2}{2(10)} + 30 \\ &= 40 \quad (^\circ\text{C}) \end{aligned}$$

(2) 由上兩式可得

$$\begin{aligned} \frac{T - T_w}{T_0 - T_w} &= \frac{\frac{\dot{q}L^2}{2k} \left(1 - \frac{x^2}{L^2}\right)}{\frac{\dot{q}L^2}{2k}} = 1 - \frac{x^2}{L^2} = 1 - \frac{x^2}{(1)^2} \\ &= 1 - x^2 \end{aligned}$$



例題 4

A plane wall of thickness 0.1 m and thermal conductivity 25 W/(m·K) having uniform volumetric heat generation of 0.3 MW/m³ is insulated on one side, while the other side is exposed to a fluid at 92°C. The convection heat transfer coefficient between the wall and the fluid is 500 W/(m²·K). Determine the maximum temperature in the wall. 【台科大機械】